

Enhanced production of L-lysine from *Corynebacterium glutamicum* by mutagenesis

Thesis submitted in partial fulfillment of the requirement for the award of

degree of

MASTER OF SCIENCE

IN

BIOTECHNOLOGY

By

Himani Thakkar

(ROLL NO. 301001011)

Under The Guidance of

Dr. M.S. Reddy

Head of Department

Department of Biotechnology and Environmental Sciences



Department of Biotechnology and Environmental Sciences

Thapar University

Patiala-147004, Punjab

July 2012

CERTIFICATE

This is to certify that the thesis entitled "Enhanced production of L-lysine from *Corynebacterium glutamicum* by mutagenesis" submitted by Himani Thakkar (Roll No. 301001011) as a part of curriculum for degree of Master of Science, Department of Biotechnology and Environmental Science, Thapar University, Patiala, is a record of student's own work under our guidance and supervision. This report has not been submitted for the award of any other degree or certificate in this or any other university.



Dr. M.S. Reddy
Supervisor and Head
DBTES
Thapar University
Patiala

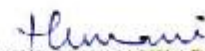


Dr. S.K. Monapatra
Dean (Academic Affairs)
Thapar University
Patiala

CANDIDATE'S DECLARATION

I hereby declare that the work which is being presented in the dissertation entitled "Enhanced production of L-lysine from *Corynebacterium glutamicum* by mutagenesis", in partial fulfillment of the requirement for the award of the degree of Masters of Science in Biotechnology, Department of Biotechnology and Environmental Sciences, Thapar University, Patiala, Punjab; is an authentic record of my own work during a period of six months from January 2012 to June 2012, under the supervision of Dr. M. Sudhakara Reddy, Head of Department of Biotechnology and Environmental Sciences, Thapar University. The matter embodied in this thesis has not been submitted in part or full to any other university or institute for the award of any other degree.

Place: Patiala


HIMANI THAKKAR

Date: 16-7-2012

List of Abbreviations

%	Percentage
μ	Micron
g/l	gram per liter
hrs.	hours
mg	milligram
min	minute
ml	millilitre
nm	nanometer
α	alpha
NTG	N-methyl-N'-nitro-nitrosoguanidine
PITC	Phenylisothiocyanate
Thr	Threonine
UV	Ultra violet
MTCC	Microbial Type Culture Collection
OD	Optical density
AEC	S-aminoethyl-L-cysteine
AK	Aspartokinase
DAP	Diaminopimelic acid pathway
EMS	Ethyl-methanesulfonate
HPLC	High performance/performance liquid chromatography

HSV	Herpes simplex virus
Met	Methionine
TEA	Triethylamine

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Introduction

For thousands of years, microorganisms have been used to supply products such as bread, beer and wine. In the early 1970s, traditional industrial microbiology was merged with molecular biology to yield more than 40 biopharmaceutical products, such as erythropoietin, human growth hormone and interferons. Today, microbiology is a major participant in global industry, especially in the pharmaceutical, food and chemical industries.

Although microbes are extremely good at producing an amazing array of valuable products, they usually produce these compounds in small amounts that are needed for their own benefit. By contrast, the industrial microbiologists screens for a strain that will overproduce a particular compound that can be isolated and marketed. After a desired strain has been found, a development program is initiated to improve titers by modification of culture conditions using mutation and recombinant DNA techniques. The main reason for the use of microorganisms to produce compounds that can otherwise be isolated from plants and animals, or synthesized by chemists, is the ease of increasing production by environmental and genetic manipulation; many fold increases have been recorded for small metabolites.

Amino acids have many special properties which make them very valuable, as for example their contribution to nutrition, the taste, the chemical features and their importance in physiological activities. Amino acids are the building blocks of proteins, they are important intermediates on the pathway from the genetic to the protein level. This demands the large production of amino acid (Leuchtenberger 1996).

It is possible to synthesize all amino acids in the traditional chemical way but amino acids produced by microbial process are generally L-forms. The stereospecificity of the amino acids produced by fermentation makes the process advantageous compared with synthetic process. Microorganisms employed in microbial process for amino acid production are divided into 4 classes; wild-type strain, auxotrophic mutant, regulatory mutant and auxotrophic regulatory mutant.

Lysine, due to inability of humans and animals to synthesize it, is designated as an essential amino acid. It must be obtained through the diet. However, lysine is known as a first limiting amino acid in feed.

A model microorganism for the overproduction of amino acids is *Corynebacterium glutamicum*, because of its simplified metabolic pathways for the production of amino acids (Lee *et al.* 2003; Gomes *et al.* 2005). For this reason it is easier to develop a new strain with changed metabolic fluxes in order to produce L-lysine. The production of L-lysine, an important animal food additive, is performed with overproducing strains of *Corynebacterium glutamicum* (Eggeling *et al.* 1999).

Random mutagenesis is a powerful tool for studying the effects of a large number of permutations of a particular DNA sequence and its encoded products. It is a basis method in biochemistry to improve the abilities of microorganisms. Mutation is performed by the use of highly potent chemical mutagens for bacteria like NTG (N-methyl-N'-nitro-nitrosoguanidine) and EMS (ethyl-methanesulfonate) or ultraviolet (UV) radiations.

Effects of UV radiation on DNA is the formation of dimers of any two adjacent pyrimidine bases (T, thymine; C cytosine), intrastrand cyclobutane pyrimidine dimers are the predominant lesion produced by UV light. UV light can induce both base pair and frame shift mutations. The ratio of mutation to lethality is usually high and UV is relatively safe mutagen.

A major problem in microorganisms is strongly regulated biosynthesis of amino acid. The amino acid produced itself restricts the formation of necessary enzymes (feedback repression) and / or reduces the activity of key enzymes for the metabolic building pathway (feedback inhibition) (Leuchtenberger *et al.* 1998). In a suitable strain, the control mechanisms have to be deactivated. In addition, side reactions and the degradation of end and intermediate products have to be blocked. For this reason the first target is to deactivate this molecular mechanism. The method used is the random mutation following selection (Gerhardt *et al.* 1981). The treatment of cells with UV-radiation or chemical mutagens (random mutation) and the selection with structural analog of lysine is widely used. (Kase *et al.* 1974; Kumar *et al.* 2002). The mutants obtained using the structural analog are regarded as regulatory mutants because of the alteration in regulatory mechanism i.e. feedback inhibition and repression of the metabolic pathway. An auxotrophic mutant is one which has lost the capability of synthesizing a metabolite required for growth. An auxotroph that requires

threonine and methionine for growth was selected for lysine production because due to release of feedback mechanism, the side reactions are blocked and the intermediate is channelled only to lysine production.

OBJECTIVES

1. Development of thialysine (AEC) resistant and auxotrophic mutants by random mutagenesis via UV light.
2. Mutants screening to analyse lysine concentration and its comparison with wild type strain.

Review of literature

2.1 Lysine: History, chemistry and biological activity

Lysine is first mentioned in late 19th century by the German chemist Drechsel (Greenstein1961). Lysine was firstly obtained from casein, but Drechsel, assuming that the compound is urea obtained from unknown source, gave the name 'lysitine' (greek word for loosing). A few years later was established that 'lysitine' is a mixture of lysine and arginine. In order to distinguish pure compounds obtained in the mixture, the name 'lysine' was given by Drechsel in 1891 to diaminocaproic acid, the next analog to ornithine. Lysine (Lys, K) is a basic and branched amino acid with six carbons and two amino groups on terminal ends.

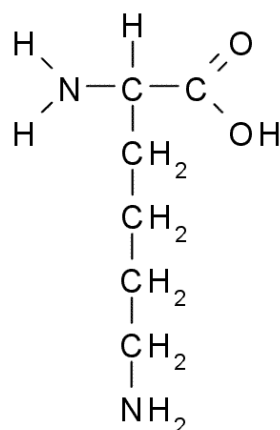


Figure 2.1: Structure of lysine

The systematic name for lysine is (S)-2, 6-diaminohexanoic acid with no tautomers known, formula C₆H₁₄N₂O₂ and structure is represented in Figure 2.1. Low pK_a value of the carboxylic group (2.16) and high pK_a of the ε amino group suggests that its primary amine (4-aminobutyl) functional group is protonated at physiological pH (≈ 7.4) allowing it to act as a donor in hydrogen bonding and/or as a general base in catalysis. Lysine is a charged, polar amino acid and its aqueous solution never assumes neutral charge. Its asymmetrical structure suggests optical activity; lysine has two enantiomers: leve (L, left) and dexter (D, right). Only L form (L-lysine) is biologically active, i.e. for protein synthesis.

Lysine is typically involved in the following reactions: amine acylation, the ninhydrin reaction, carboxylic acid esterification, and specific oxidation. One can emphasize ninhydrin reaction and amine acetylation as an important feature from the prospective of the biological function of lysine. The ninhydrin reaction is a basis for the majority of chemical assays used for determination of lysine (Vogel and Shimura 1971).

Acetylation of the lysine amino groups is chemically analogous to the acetylation of the N terminus. Functionally, the acetylation of lysine residues is used to regulate the binding of proteins to nucleic acids. The cancellation of the positive charge on the lysine weakens the electrostatic attraction for the (negatively charged) nucleic acids (Voet and Voet 1990).

According to the chemical properties, the charge and basic character of a side chain (or changes on it) are responsible for the biological activity of lysine. An important role of lysine plays in metabolism is in collagen formation. It has been known that collagen biosynthesis involves post-translational modifications of the initial polypeptide chain. Intracellular modification consists of hydroxylation of lysine and proline residues followed by glycosylation of hydroxylysine residues to galactohydroxylysine, chain association, disulphide bonding and formation of the triple helix (Oikarinen *et al.* 1976). Procollagen-lysine-5-dioxygenase (lysyl hydroxylase) catalyzes hydroxylation of lysine to hydroxylysine and it is the key enzyme in collagen formation requiring vitamin C as a cofactor. Having influence on collagen formation, lysine, proline and vitamin C indirectly affect function of various tissues, and therefore, lack of these ingredients in the diet can cause serious damage and dysfunction in metabolism (Saha *et al.* 2005).

L-lysine plays an important role in many biological processes; that is the reason why it is regarded as key element in health and nutrition of animals (Oh *et al.* 1993). It also excites the cell division (Zelder *et al.* 2005) and is necessary for the carnitine production, a component vital to convert fatty acids into simpler compounds and energy and facilitating the lowering of blood cholesterol, which is important for proper body functioning. The use of L-lysine can also prove helpful to overcome heart symptom like angina pectoris. L-lysine is an essential ingredient to clean arteries, which is very important for cancer prevention.

Much of the research on the role of lysine has been directed to its effect in the treatment of herpes simplex virus (HSV). Having an essential role in HSV replication, it was found that arginine promotes viral infection (Inglis 1968) and biosynthesis of Infected cell protein 8(ICP8), a DNA-binding protein in HSV (Ruyechan and Olson 1992).

The biochemical basis for successful treatment of HSV I and II with lysine is that the similar structures of lysine and arginine make them each other's antagonists. Indeed, lysine inhibits the replication of HSV (Loh and Oie 1969). To date, numerous reports have shown that lysine positively affects treatment of HSV I and II and therefore, diet enriched in lysine is highly recommended. However, high concentration of lysine is effective only if concentration of arginine is low in the medium (Maggs *et al.* 2000) implying that successful treatment (and prevention) against HSV depends on lysine–arginine ratio rather than on solely lysine rich diet. Finally, the most general biological activity of lysine is its incorporation into proteins that serve as hormone, enzymes and antibodies in higher animals and humans.

2.2 Lysine in food

Considering that lysine metabolism is the same in humans and higher animals, it is expected that its function and benefits in humans are identical to those in animals. Therefore, infants (3-6 months) require high amounts of lysine, 97 mg/kg of body weight compared to children (10-12 year) who require 44 mg/kg of body weight, due to its role in collagen formation and consequently, growth. Adults, on the other hand, require approximately 12 mg/kg of body weight.

Human diet seems more versatile than animal diet, consisting of fruits, vegetables, meats, dairy products and sweets. Lysine is readily found in Atlantic fish, soy and egg white, which are the richest sources of lysine. If one takes into account the food groups, lysine can be obtained through meats (especially white meat), soy and dairy products easier than through vegetables and fruits. Lysine toxicity may lead to diarrhea and abdominal cramps. However, this is not frequently reported and it is associated with uptake of extremely high doses of lysine, 15-40 g per day (Foster 2008).

2.3 Methods of lysine synthesis

Methods of lysine production are chemical synthesis, enzymatic synthesis, fermentation. Bulk of the production occurs by fermentation.

2.3.1 Chemical method of lysine synthesis

Caprolactum is being used as a starting material for the synthesis of lysine in recent years because of its availability and structural advantages (Roger Tull 1964). Introduction of amino group into caprolactum by direct monochlorination in the alpha position is not successful, therefore in contrast to caprolactam, N- benzoyl- ϵ -caprolactam is used.

Figure 2.2 shows the process of chemical synthesis of lysine, N-benzoyl- ϵ -caprolactam (II) undergoes monochlorination smoothly with sulfuryl chloride to give N-benzoyl- α -chloro- ϵ -caprolactam (III). N- benzoyl- ϵ -caprolactam is hydrolysed with sodium hydroxide to form ϵ -benzamide- α -chlorocaproic acid (IV), this is then converted to DL lysine by amination and hydrolysis.

Acidic hydrolysis of N-benzoyl- ϵ -caprolactam (III) provide another route to DL-lysine. Concentrated sulphuric acid cleaves benzoyl group to form α -chloro- ϵ -caprolactam (VI) which is then converted to lysine by ammonolysis followed by hydrolysis.

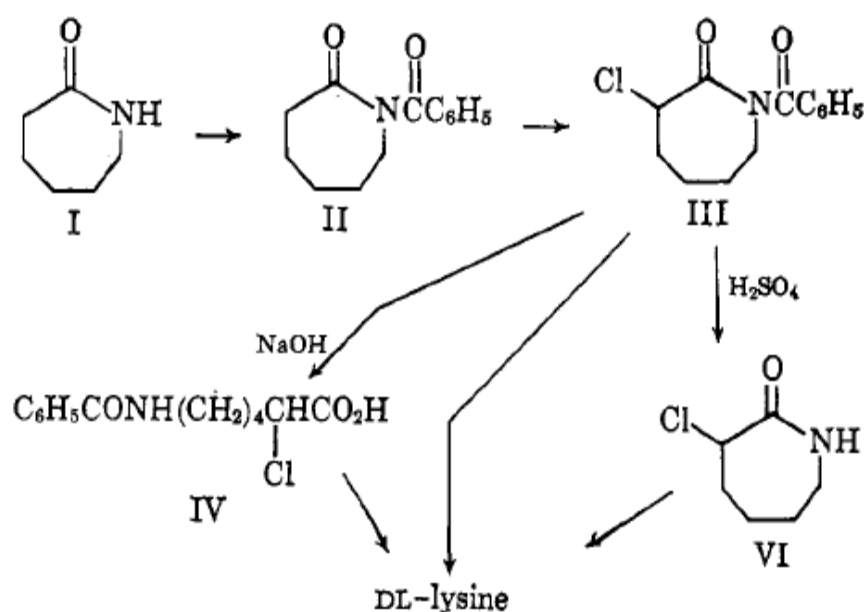


Figure 2.2: Lysine synthesis by chemical method

2.3.2 Enzymatic method of synthesis

Fukumura (1976) established an enzymatic process for the production of L-lysine using DL- α -amino-caprolactum(AAC) as a starting material, DL-amino- α -caprolactam is obtained from cyclohexene.

The process is composed of two enzymatic reaction (Figure 2.3)

1) A 10% DL- α -amino-caprolactum(produced chemically) pH 8.0 is treated with 1.0% (w/v) acetone-dried cells of *Cryptococcus laurentii* and of *Achromobacter abae* for 24 hrs at 40°C to obtain L-lysine.

2) The D- α -amino- caprolactam,which is left behind is converted to L-amino caprolactum by specific racemase enzyme so that lysine is the sole product of the process. In this process D- α -amino-caprolactam is racemized to L- α -amino-caprolactam by racemase of *Achromobacter abae*, which is further hydrolysed by a hydrolase from *Cryptococcus laurentii*.

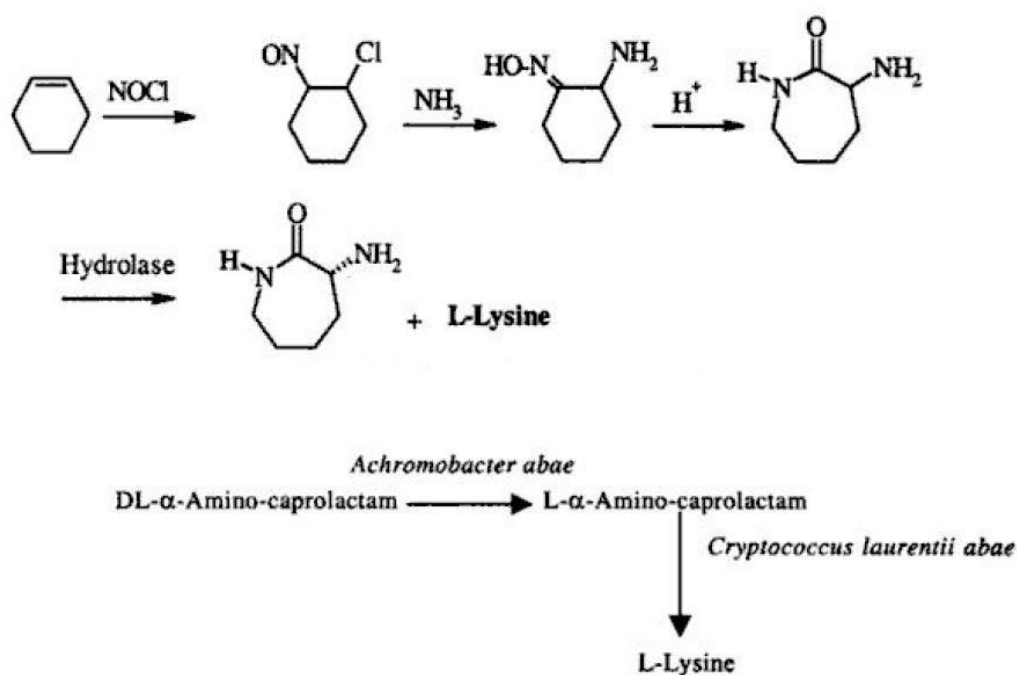


Figure 2.3: Lysine synthesis by enzymatic method

2.3.3 Biosynthesis of lysine and its regulation

Lysine biosynthesis occurs in bacteria, fungi, algae and higher plants. Higher animals and humans have lost the ability to synthesize lysine. However, the biosynthetic pathways for lysine synthesis in the above mentioned species differ (Caspi *et al.* 2008).

Lysine biosynthesis in microorganisms and plants occur via two distinct pathways: the diaminopimelic (DAP) pathway and α -aminoadipic acid (AAA) pathway (Vogel 1964). It was firstly suggested that the consistency of their distribution over a broad range of biological species implied that this dichotomy was probably not the result of a gene transfer between the species. Since that diaminopimelic acid is a bacterial cell wall constituent, most bacteria synthesize lysine via DAP. On the other hand, fungi that typically contain chitin in their cell wall, synthesize lysine via AAA.

2.3.3.1 Diaminopimelic (DAP) pathway

The DAP pathway is characteristic of bacteria, algae, Oomycetes, Myxomycetes, Hyphochytrids and higher plants. It is a branched pathway where lysine has been synthesized along with threonine, methionine and isoleucine, which are designated as aspartate family amino acids. The first four steps in DAP biosynthetic pathway. These steps are common in all bacteria, plants, algae, Oomycetes, Myxomycetes and Hyphochytrids (Weinberger *et al.*, 1970). Enzymes and corresponding genes are designated as in *Corynebacterium glutamicum*. Lysine biosynthesis pathway in *Corynebacterium glutamicum* (Figure 2.4).

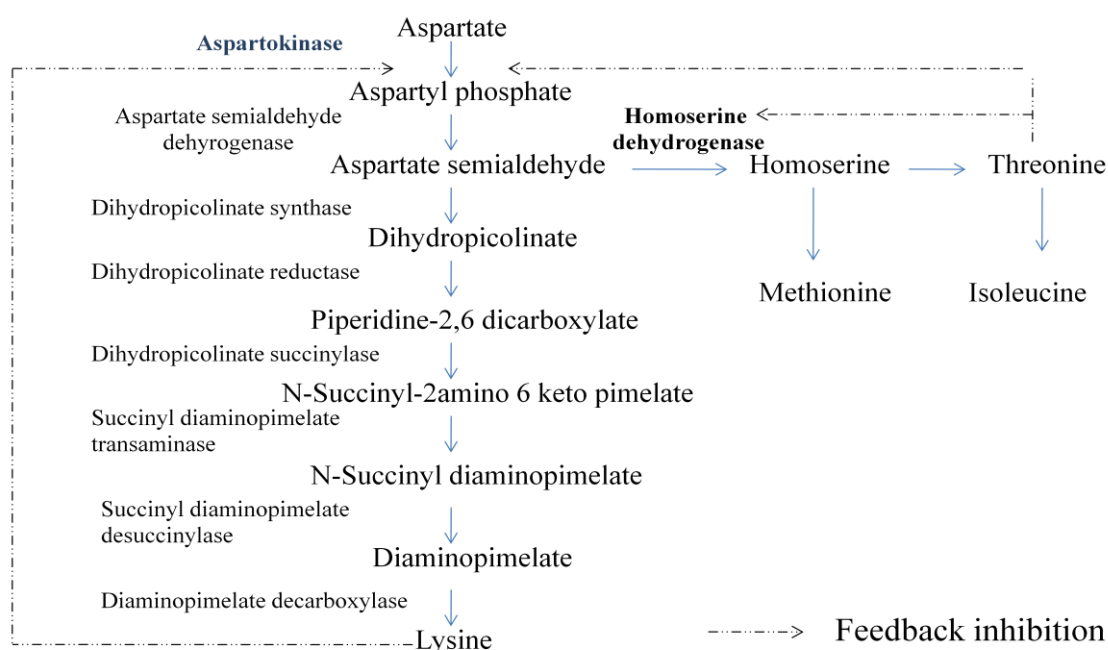


Figure 2.4: Lysine biosynthesis pathway in *Corynebacterium glutamicum* (Wehrmann *et al.* 1998)

The DAP pathway is typically regulated by feed-back inhibition, where products inhibit and/or repress the key enzyme in the pathway. In this case, aspartokinase is subjected to multiple feed-back inhibition and/or repression. Due to complexity of the pathway, aspartokinase usually exists in the form of isozymes, which are inhibited and/or repressed by lysine, threonine, methionine or subjected to concerted inhibition of two or more aspartate family amino acids (Kalinowski *et al.* 1991; Malumbres and Martin 1996). The number of isozymes and manner of inhibition/repression vary among the species. Isoleucine seldom has influence on aspartokinase, in spite of the fact that it is the final product of the biosynthesis; it rather influences threonine deaminase, which is the first step in the branch of the pathway that leads to isoleucine solely. Homoserine is the starting point for making threonine and isoleucine as well as methionine. The major control points for the metabolic flux to individual amino acids occurs at the level of aspartokinase and homoserine dehydrogenase. (Blombach *et al.* 2009).

It is known that lysine biosynthesis genes are scattered along the chromosome in *E. coli*, enterobacteria, members of Pasteurellales and Vibrionaceae and *Shewanella oneidensis*. In contrast, in Gram-positive bacteria belonging to the *Bacillus/Clostridium* group, lysine

biosynthesis genes were found within clusters potentially forming an operon (Rodinov *et al.* 2003). The highly conserved metabolite-binding RNA domain designated as *LYS* element predominantly regulates either single *lysC* (encoding aspartokinase) or *lysA* (encoding diaminopimelate decarboxylase) genes or a composite lysine operon. Therefore, over-expression of these genes is directly due to mutation(s) in *LYS* element. Grundy *et al.* (2003) have confirmed the hypothesis showing that in *B. subtilis* lysine directly promotes transcription termination causing structural shift in the *LYS* element of *lysC*. In contrast, *LYS* element in Gram-negative bacteria appeared to be regulated at the level of translation initiation rather than transcription termination.

2.4 *Corynebacterium glutamicum*

In 1957 Kinoshita *et al.* isolated a bacterial strain which was able to overproduce L-glutamic acid in minimal media with glucose as carbon source and release the product in the extracellular environment. The isolated soil bacterium was named *Corynebacterium glutamicum*. In taxonomic terms it belongs to the family of *Corynebacteriaceae*. Its cell wall formation is very characteristic (gram positive), especially the existence of mycolic acids which surround the entire cell as a structured layer (Eggeling *et al.* 2003). The wild type strains are mostly able to grow aerobically on basic minimal media containing a carbon source like glucose, phosphate, sulphate, ammonia and in addition biotin due to the fact that this bacterial species is completely biotin deficient (Stansen 2005). Furthermore *Corynebacterium glutamicum* is immobile and non-sporulating. Since the isolation in 1957 high amounts of L-glutamic acid have been produced with new developed or advanced strains of this species. Figure 2.5 shows the rod shaped structure of *Corynebacterium glutamicum*

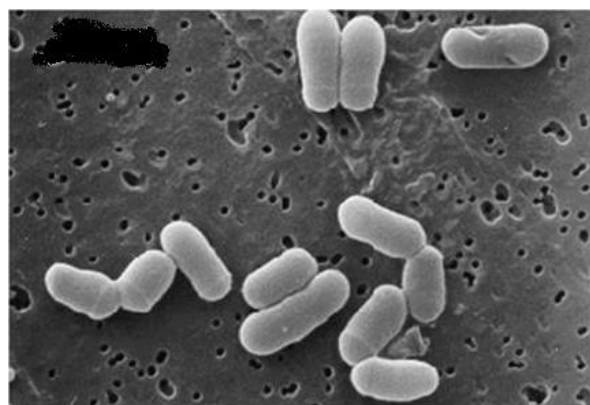


Figure 2.5: *Corynebacterium glutamicum* (Courtesy of Michael Bott / Research Center Jülich)

The cell wall of *Corynebacteriaceae* has a special structure which is different from other gram positive bacteria; The peptidoglycan layer is connected to the heteropolysaccharide arabinogalactan (Figure 2.6). The external mycolic acid layer is linked again with the arabinogalactan (Eggeling et al. 2003).

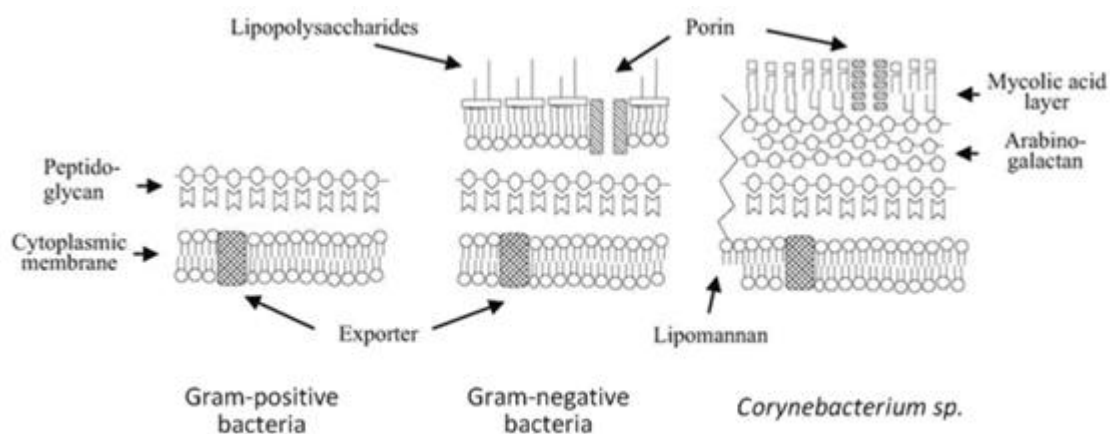


Figure 2.6: Formation of the *Corynebacterium glutamicum* cell wall (right) in comparison to gram-positive (left) and gram-negative bacteria (middle) (Eggeling et al. 2003)

Because of many experiences the scientists gained over the last decades about this organism and its metabolic fluxes in context of amino acid production, *Corynebacterium glutamicum* has become the most important bacterial strain for amino acid overproduction (Schmid 2002). It has been observed that the regulatory system is much more simple than that of *Escherichia coli* (Tosaka et al. 1986). There is information of the production of L-glutamic acid (Kinoshita et al. 1961), L-phenylalanine (e.g. Wartenberg 1989), L-lysine (Eggeling et al. 1999), L-valine (Blombach et al. 2007) and L-methionine (Kumar 2002) using strains of *Corynebacterium glutamicum*.

2.5 Strain improvement

After the discovery of its ability to produce and excrete amino acids (Kinoshita et al. 1957), *C. glutamicum* was used to establish a biotechnological production process for several amino acids. Through the years various methods for strain engineering have been developed to create more efficient production strains.

2.5.1 Random mutagenesis

The first production strains were created within a few years after the discovery of *C. glutamicum* using an iterative procedure of random mutagenesis with UV light or chemical mutagens and subsequent strain selection (Nakayama *et al.* 1978).

Ultraviolet rays are one of the widely used physical induced mutagen to make mutants.

UV is normally classified in terms of its wavelength.

- UV-C (180-290 nm): "germicidal"--most energetic and lethal, it is not found in sunlight because it is absorbed by the ozone layer
- UV-B (290-320 nm): major lethal/mutagenic fraction of sunlight
- UV-A (320 nm--visible): "near UV"--also has deleterious effects (primarily because it creates oxygen radicals) but it produces very few pyrimidine dimers.

When deoxyribonucleic acid (DNA) is exposed to UV light (254nm), the most frequent DNA damage, or lesions, results at dimers of any two adjacent pyrimidine bases (T, thymine; C cytosine) causing T-T, C-T, and C-C dimers, but T-T dimers are the most common cyclobutane pyrimidine dimers (Figure 2.7). Another type of DNA damage is the 6-4 pyrimidine-pyrimidine photoproducts (Goosen and Moolenaar, 2008). The handling of UV radiation in screening systems is far easier process .Usually UV rays around 250 nm are deployed in experiments.

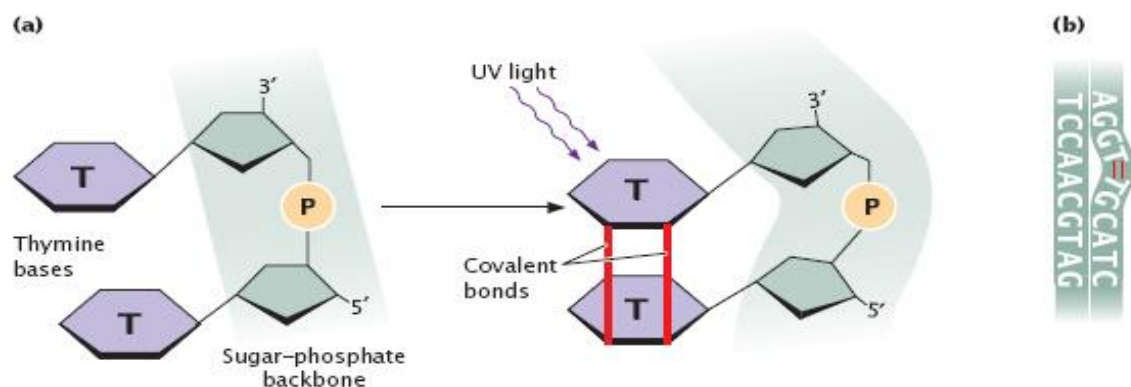


Figure 2.7: (a) Pyrimidine dimers results from UV light ,(b) distorted DNA (Source: Genetics: a Conceptual Approach, 2nd ed.)

The key to success in these days was the use of toxic lysine analogues, such as S-(2-aminoethyl) cysteine (AEC) or thialysine (Figure 2.8), to screen for feedback resistant strains (Nakayama and Araki 1973).

other amino acids, vitamins and resistance to other anti-metabolites were obtained. (Kelle *et al.* 2005).

In auxotrophic mutants the inhibition of homoserine synthesis, by nullifying the activity of the homoserine dehydrogenase enzyme, results in the release of the feedback inhibition by threonine and lysine on aspartate kinase. Consequently, the aspartic semialdehyde produced can proceed to lysine through the lysine biosynthetic pathway, where no further inhibition has been detected (Figure 2.10). Lysine overproduction by development of mutants of many other bacteria species have also been done (Samanta 1988; Sambanthamurthi 1984)

The isolation of auxotroph was achieved using the penicillin enrichment technique, (Fitzgerald, 1975). Penicillin kills only growing cells and therefore, if the survivors of a mutation treatment were culture in a medium containing penicillin and lacking the growth requirement of the desired mutant only those cells unable to grow would survive i.e. the desired auxotroph. These cells are then removed from the penicillin broth and resuspended in medium containing the requirement of the desired auxotroph.

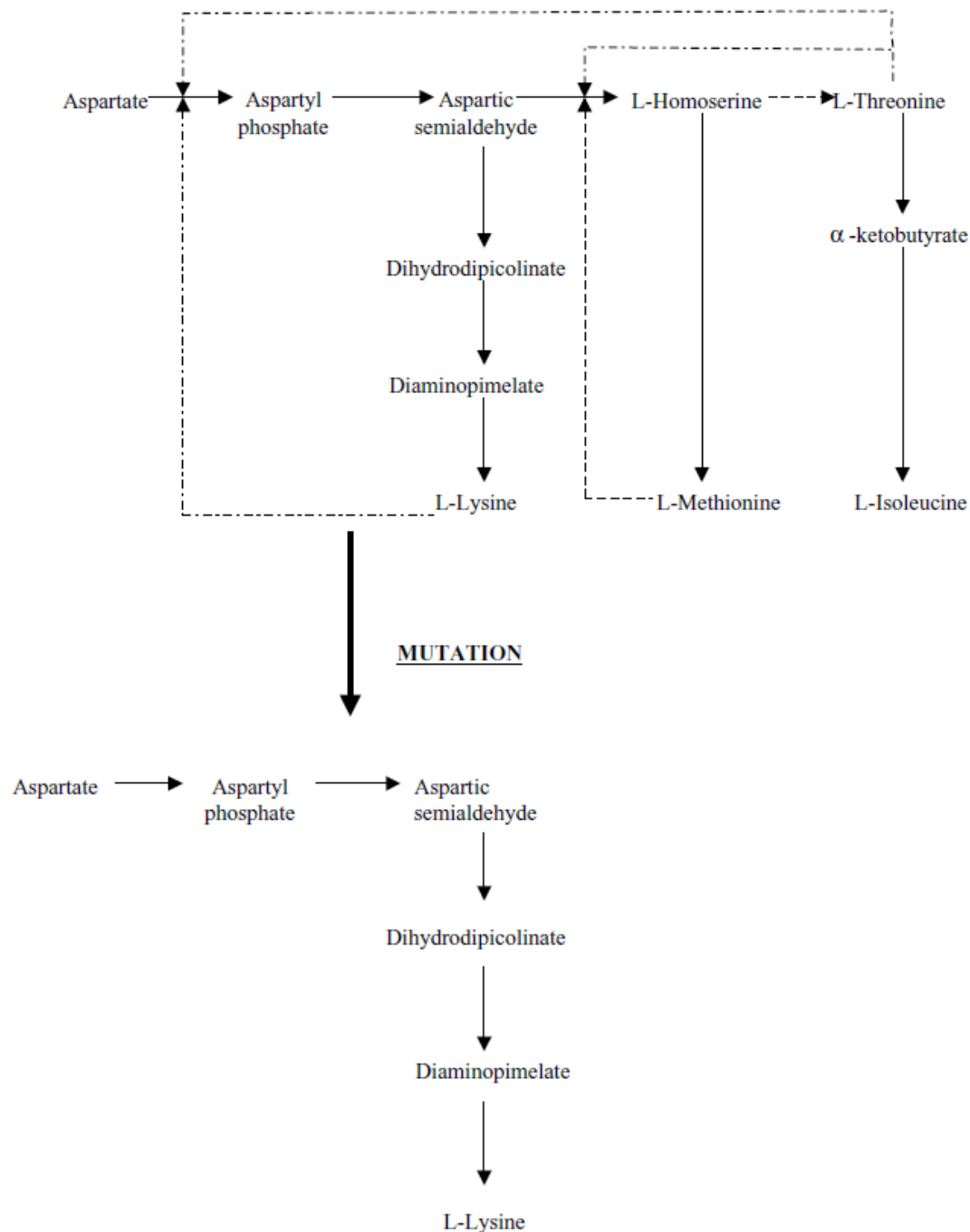


Figure 2.10: Deregulation of lysine synthesis in auxotrophs (Nakayama, 1985)

The subsequent mutants from such a strain genealogy exhibited a stepwise improvement of production (Schrumpf *et al.* 1992; Wittmann 2004). Remarkable production properties such as a conversion yield up to 50% were achieved with such classically derived strains (Ikeda 2003). There were some drawbacks of classical method i.e. the additional nutrient requirement and the weak stress tolerance, due to the large number of undesired mutations

accumulated during strain development (Ohnishi *et al.* 2002), display, however, severe disadvantages of conventional production strains and stimulated targeted approaches for strain optimization. After the gene targets improving lysine production had been identified it became possible to introduce mutant alleles of these genes isolated from the classically obtained producer strains into the wild type to generate stable and stress-tolerant lysine producer strains without additional nutrient requirements (Hayashi *et al.* 2006a; Ohnishi *et al.* 2002).

The excretion of amino acids is an important factor for overproducing microorganisms. If the product is accumulated intracellularly, an additional step in downstream processing is necessary, the cell disruption. In addition to the ubiquitous inner lipid bilayer, the cell envelope has an outer lipid layer which contains mycolic acids and is probably also organized as a bilayer. During export, the amino acid has to pass these different layers of the cell wall. Molecular investigations have now identified the L-lysine exporter LysE and the L-threonine exporter ThrE which are localized in the inner cytoplasmic bilayer (Eggeling, Sahm, 2005). The L-lysine exporter also exports L-arginine. Its expression is regulated by an elevated concentration of the cell-internal amino acid. Export thus represents a new bacterial mechanism for regulating the cellular amino acid balance. The export of L-glutamic acid is still enigmatic, although the outer lipid layer seems to play a major role in the efflux of this amino acid. It is assumed that the ultimate target is primarily the outer mycolic acid layer. For *Corynebacterium glutamicum*, which is a biotin deficient strain, the amount of this vitamin in minimal media is an important factor to get optimal excretion (Clement *et al.* 1986).

2.5.2 Metabolic Engineering of Lysine Biosynthesis

The possibility to perform targeted genetic modifications through developments of molecular biology and genetic engineering tools initiated a number of efforts towards rational optimization to *C. glutamicum* (Ohnishi *et al.* 2002). Logically, many of these studies have focussed on the optimization of the flux through the lysine biosynthesis by directly modifying enzymes of the pathway. The modification of three of the enzymes, i.e. aspartate kinase (LysC), dihydrodipicolinate synthase (DapA) and the lysine exporter (LysE), was especially valuable with respect to improvement of lysine production (Nishida 1997). Aspartate kinase is the key enzyme with regard to metabolic control of the lysine pathway as it is subject to a feedback inhibition by threonine and lysine (Kalinowski *et al.* 1991; Malumbres and Martin 1996). Different point mutations in the *lysC* gene, i.e. in the region coding for its regulatory

β -subunit, have been shown to release the enzyme from feedback control and lead to enhanced lysine formation (Cremer *et al.* 1991; Kalinowski *et al.* 1991). Similarly, also overexpression of the aspartate kinase gene stimulated production (Jetten *et al.* 1995). Today, the release of aspartate kinase from feedback control is regarded as one of the most important features of industrial lysine producer strains. This is also underlined by the various patents claiming different amino acid exchanges in this enzyme.

Plasmid encoded amplified expression of the *dapA* gene significantly increases lysine (Cremer *et al.* 1991; Eggeling *et al.* 1999; Pisabarro *et al.* 1993). Amplification of *dapA* expression was further achieved through an extensive mutation of the promoter sequence, whereby a hot spot was discovered at the – 10 region (de Graaf *et al.* 2001). A striking discovery with respect to lysine production was the discovery of the lysine exporter (LysE) and the subsequent overexpression of the *lysE* gene which resulted in an increased lysine secretion rate (Bellmann *et al.* 2001; Koffas 2005). The recently performed expression of *lysE* from *C. glutamicum* in a *Methylophilus methylotrophus* lysine producing strain was shown to also improve lysine production from methanol by this organism (Gunji and Yasueda 2006). Summarizing, the importance of engineering enzymes of the lysine pathway for efficient lysine production is underlined by the fact that today every single gene of the lysine biosynthetic pathway is covered with one or several patents by the major players in the field.

Materials and method

3.1 Microbial strains: Two bacterial strains procured from MTCC were used for this study

Corynebacterium glutamicum MTCC1815

Corynebacterium glutamicum MTCC2745

3.2 Media compositions

Complete media (Composition g per litre)

For *Corynebacterium glutamicum* strain MTCC 1815

For MTCC 2745

Casein peptone	10g	Beef extract	1g
Yeast extract	5g	Yeast extract	2g
Glucose	5g	Peptone	5g
NaCl	5g	NaCl	5g
Water	1000ml	Water	1000ml
pH	7.2	pH	7.2

Minimal media

Glucose	2g
Ammonium sulphate	1g
Dipotassium hydrogen sulphate	7g
Potassium dihydrogen sulphate	3g
Sodium citrate	0.5g
Magnesium sulphate	0.1g
Biotin	10µg
Thiamine hydrochloride	20µg

Above components were dissolved in 1000 ml water and pH was adjusted to 7.2.

Screening media for lysine production

Glucose	5g
Ammonium sulphate	1g
Dipotassium hydrogen sulphate	7g
Potassium dihydrogen sulphate	3g
Calcium carbonate	10g
Ferrous sulphate seven hydrate	2mg
Manganese chloride tetrahydrate	2mg
Magnesium sulphate	0.1g
Biotin	10µg
Thiamine hydrochloride	20µg
Water	1000ml
pH	7.2

For screening of auxotrophic mutant, 0.4 g of amino acid of desired auxotroph was added. Glucose was separately sterilized as 40 % stock solution, Biotin, thiamine and amino acids were sterilized through 0.22 µm filter.

3.3 Reagent for estimation of lysine

Ninhydrin ferric reagent (Hwang *et al.* 1995) was prepared as follows

Reagent A: Methylcellosolve (373ml) and 30 ml of 50% (w/w) ferric chloride solution were added to 600 ml 0.1M KCl solution which was adjusted by 1N HCl to a pH of 1.0.

Reagent B: Ninhydrin (1g) was dissolved into 100ml 0.1M KCl which was adjusted by 1N HCl to a pH1.0.

3.4 Procedure

3.4.1 Mutagenesis

1. Lyophilised cells of *Corynebacterium glutamicum* were revived by inoculating in broth and streaking on the agar plates.
2. Loop of cells were then inoculated in the broth at 30°C on shaking incubator for 24 hrs.
3. 5 ml of culture broth (of OD₆₀₀ 0.3) was irradiated in small Petri plates for different time periods viz. 2, 4, 6, 8, 10 minutes at exposure distance of 20 cm (Dose 37mW/cm²/sec).
4. After exposure 100 µl of culture broth with dilution 10⁻⁴ was spread on the agar plates and incubated at 30 C for 24 hrs.
5. Colonies were counted from these plates to check the survival rate.

3.4.2 Development and isolation of thialysine resistant mutants

1. Loop of cells were inoculated to 20 ml minimal media and incubated at 30°C on shaking incubator for 24 hrs.
2. 5 ml of the culture broth (OD₆₀₀ 0.3) was irradiated for 6min at exposure distance of 20cm (Dose 37 mW/cm²/sec)
3. UV irradiated cells were smeared on minimal agar plus 2 mg/ml thialysine and incubated at 30°C for 3 days.
4. Thialysine resistant mutants were picked and inoculated in 20 ml screening media at 30°C for 72 hrs.
5. Culture broth was then centrifuged at 10,000 rpm at 4°C and supernatant was analysed for lysine production by ninhydrin ferric reagent.

3.4.3 Development and isolation of auxotrophic mutants

1. Exponentially growing cells of thialysine resistant mutant were irradiated by UV for 6 min at exposure distance of 20 cm.
2. To 1 ml UV irradiated cells, 100 units of penicillin G was added and incubated for 20 hrs on shaking incubator at 30°C.
3. After 20 hrs, 50 units of penicillinase was added and left for 10 min.
4. 0.2 ml of culture was spread on complete agar plates and minimal agar, minimal agar plus threonine, minimal agar plus threonine and minimal agar plus methionine and threonine plates and incubated for 48 hrs.

5. Colonies that did not grow on minimal agar but on minimal agar plus amino acid of the respective auxotroph were isolated.
6. Auxotrophic mutants were screened for lysine production by inoculating in screening media for 72 hrs.
7. Samples were taken, centrifuged and examined for lysine concentration.

3.5 Analytical analysis

3.5.1 Qualitative analysis of lysine

For qualitative analysis paper chromatography technique was used (Momose and Takagi, 1978)

1. Solution of the sample (supernatant) and standard were spotted on the Whatman No.1 filter paper.
2. Spots were air dried at room temperature and then the paper was dipped in the solvent (mixture of 40:10:50 butanol:acetic acid:water)
3. The solvent was allowed to run till it reaches more than half of the paper.
4. Paper was then air dried and uniformly sprayed with 0.5% ninhydrin in 95% acetone.
5. After air drying paper was kept at 65°C for 15 min in the oven.
6. Position of amino acid was indicated by the formation of a well defined coloured spots. The amino acid in the samples was identified with the spot of standard.

3.5.2 Quantitative analysis

Lysine was assayed by ninhydrin ferric reagent method.

1. Culture broth was centrifuged at 10,000 rpm at 4°C.
2. To 20µl of the supernatant 0.66 ml of reagent A and 0.37 ml of reagent B was added.
3. The mixture was heated at 100°C for 20 min in water bath and then cooled.
4. 4ml dimethyl sulphoxide was added and thoroughly mixed to solubilize the coloured product.
5. After mixing, 6 ml of water was added and again mixed.
6. Absorbance was measured at 470 nm against blank (without culture supernatant).
7. Lysine concentration was calculated with the reference to a calibration graph plotted from the result obtained by standards containing 0.1, 0.3, 0.5, 0.7 and 0.9 g/l lysine.

3.5.3 HPLC analysis

Redrying solution: 2:2:1 mixture of ethanol:water: triethylamine (TEA) (v/v), 5 mM Na₂PO₄ buffer, pH 7.4 containing 5% acetonitrile.

Derivatising solution: mixture of 7:1:1:1 ethanol: water: TEA: phenylisothiocyanate (PITC) (v/v).

Table 3.1: Components of HPLC system and conditions required for optimised separation

Process performance	Gradient, temperature maintained at 38°C
Sample volume	10µl
Mobile phase	A: 150 mM CH ₃ COONa ₃ H ₂ O, 0.05% TEA, and 6% acetonitrile, pH 6.4 B: 6:4 acetonitrile: water (v/v) (Both eluents were sparged with ultra pure helium gas for 10 min before use)
Flow rate	1ml/min
Column	The reversephase column used was a Pico-Tag (3.9 mm length, 150 mm diameter), dimethyloctadecylsilyl bonded amorphous silica, with an inline column filter.
Components of HPLC system	UV detector (254nm)

PROCEDURE

Pre column derivitization

1. Sample was diluted by dissolving the 990 µl in 10 µl miliQ.

2. Standard and samples (supernatant) were neutralized by adding 10 μ l redrying solution and mixing well with a vortex stirrer. They were dried under vacuum for 20-30 min.
3. Redrying was done by adding redrying agent for 15-20 min.
4. Derivatization was performed by adding 20 μ l of derivatising agent and mixing well with a vortex stirrer. The reaction between PITC and the hydrolysate to produce phenylthiocarbamyl (PTC) amino acids was allowed to complete for 20 min at room temperature. Samples were then completely dried under vacuum for 1hr and stored in a freezer.

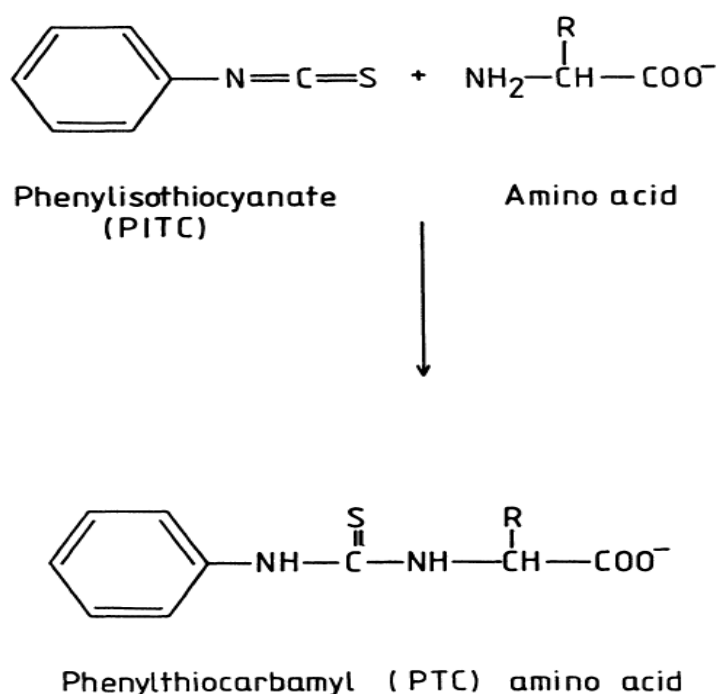


Figure 3.2: Reaction of amino acid with phenylisothiocyanate during precolumn derivatisation

HPLC Analysis

1. Phenylthiocarbamyl amino acids (Figure 3.2) in each sample and standard were dissolved from the dried matrix by vortex mixing with 200 μ l of sample diluent.
2. The fluid was then filtered through a 0.2 μ m membrane.
3. Samples were reconstituted one at a time due to the PTC amino acid sensitivity to light and ambient temperature.

4. 10 μ l of sample and 5 μ l of standard were injected and analyzed with an HPLC system equipped with a column heater, autosampler, variable wavelength detector, and a data acquisition software controller.
5. The PTC amino acids were separated and eluted by a gradient resulting from mixing eluents A and B. The flow rate was 1 ml/min throughout, and the gradient consisted B at 5.5 min, 54% A and 46% B at 10 min, 100% B at 10.5–12.5 min, 100% A at 13 min. The PTC amino acids eluted from column were detected at 254 nm and recorded.
6. The column was regenerated and equilibrated with eluent A for 10 min. A new and freshly reconstituted sample was injected, either by manual injector or autosampler/injector, and analyzed every 23 min.

3.6 Effect of fermentation time

The culture was inoculated in the screening media and incubated at 30°C. Lysine concentration was measured after 24, 48, 72, 96, 120 hrs. by ninhydrin ferric reagent.

3.7 Effect of different carbon sources on lysine production

Bacterial culture was inoculated in screening media with different carbon sources such as glucose, sucrose, acetate, galactose, fructose with a concentration of 50 g/l and incubated at 30°C for 72 hrs. Lysine production was analysed in different sources and compared.

Results

4.1 Effect of UV dosage on lethality level

After spreading 100 μ l of UV exposed culture on complete media agar plates, number of colonies were counted with respect to UV exposure time to determine the percentage inactivation with time. UV dosage given was 37 mW/cm²/sec.

Percentage inactivation after 6 min was 92% as shown in Table 4.1. Figure shows the survival percentage after different exposure time of UV light. UV treatment for 6 min was used to develop mutants as with 6 min 92% inactivation was achieved.

Table 4.1: Percentage inactivation with different exposure time

UV exposure time(in min)	Percent inactivation
Control	0
2	63.3 $\pm$ 3.5
4	83.0 $\pm$ 0.7
6	92.1 $\pm$ 1.0
8	0.3 $\pm$ 0.57

values are means $\pm$ standard deviation(n=3)

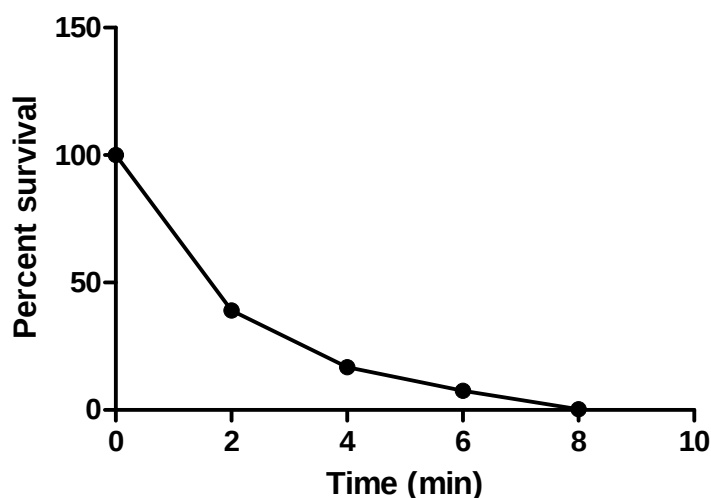


Figure 4.1: Effect of UV dose on percentage inactivation

4.2 Isolation of thialysine resistant mutants

Thialysine resistant mutants were obtained after spreading of UV irradiated cells on minimal agar plus different concentrations of thialysine after 72 hrs incubation at 30°C. Slight reduction in colony growth was observed with 1.5 mg/ml and total inhibition occurred at 2.5 and 3 mg/ml thialysine concentration. In the screening system, thialysine with concentration of 2 mg/ml in minimal medium was used as selection step after UV exposure of 6 min. With MTCC 1815 strain, 34 mutants were obtained and with MTCC 2745 strain only 4 mutants were isolated. Figure 4.2 shows the thialysine resistant mutant on minimal agar plus thialysine plates.

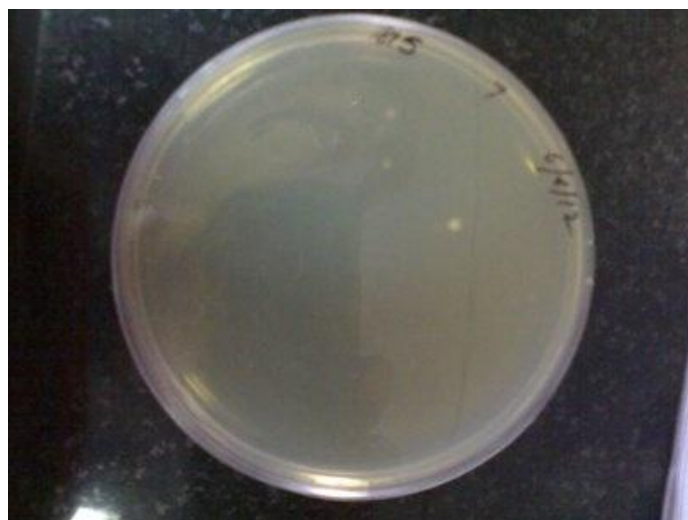


Figure 4.2: Colonies of thialysine resistant mutants on minimal agar plus thialysine plates

4.3 Comparison of thialysine mutants with wild type

Both mutants and wild type strains were inoculated in the screening medium at 30°C for 72 hrs and analysed for lysine production first qualitatively by paper chromatography and then quantitatively by ninhydrin ferric reagent method.

4.3.1 Qualitative analysis by paper chromatography

This was done to first confirm the presence of lysine in different mutants and wild type strain.

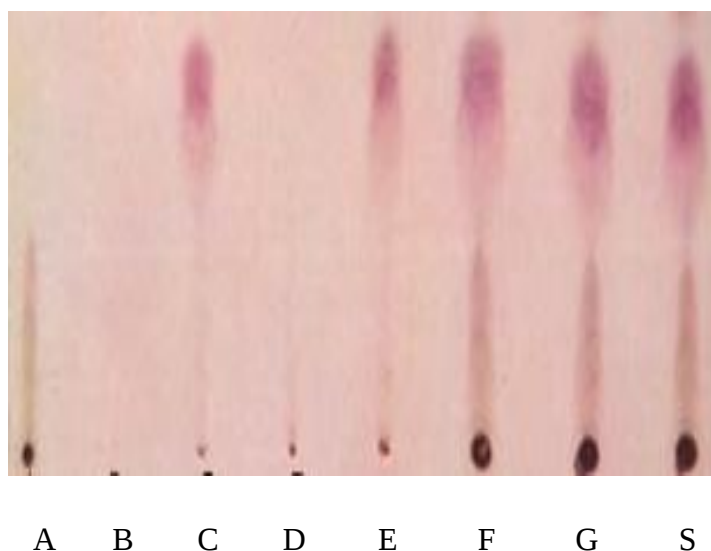


Figure 4.3: Paper chromatogram showing lysine spots of different mutants

In Figure 4.3, A – D are thialysine resistant mutants obtained with MTCC 2745 strain, E – G are mutants obtained with MTCC 1815 strain and S is reference.

It was inferred (from figure 4.3) that A, B and D mutants had no lysine production while C, E, F, G mutants showed lysine production.

4.3.2 Quantitative analysis by ninhydrin ferric reagent

Concentration of lysine in mutants (culture supernatant) and wild type strain was calculated using linear regression analysis equation derived from standard curve (Figure 4.4), $y = 1.131x + 0.071$, where y = absorbance at 470 nano meter (nm) and x = lysine (g/l).

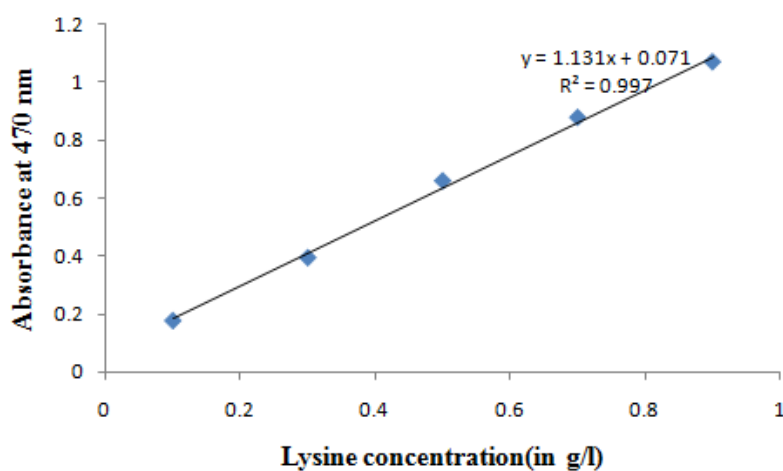


Figure 4.4: Standard Curve of Lysine Concentration

Table 4.2: Concentration of lysine in thialysine resistant mutants developed from MTCC 1815 strain

Mutants	Lysine concentration (in g/l)
Wild type MTCC 1815	0.2 ± 0.02
T 01	0.136 ± 0.01defgh
T 02	0.096 ± 0.01fghij
T 03	0.1 ± 0.03fghij
T 04	0.176 ± 0.01de
T 05	0.326 ± 0.02c
T 06	0.12 ± 0.02efghi
T 07	0.2 ± 0.01d
T 08	0.153 ± 0.01def
T 09	0.403 ± 0.005ab
T 10	0.066 ± 0.05hij
T 11	0.076 ± 0.05ghij
T 12	0.183 ± 0.01de
T 13	0.063 ± 0.02
T 14	0.16 ± 0.02def
T 15	0.12 ± 0.02efghi
T 16	0.036 ± 0.02
T 17	0.3 ± 0.01c
T 18	0.182 ± 0.02de
T 19	0.333 ± 0.01bc
T 20	0.12 ± 0.02efghi
T 21	0.076 ± 0.01ghij
T 22	0.073 ± 0.03ghij
T 23	0.14 ± 0.03defg
T 24	0.156 ± 0.01def
T 25	0.19 ± 0.01de
T 26	0.166 ± 0.03def
T 27	0.13 ± 0.01defghi
T 28	0.456 ± 0.01a
T 29	0.136 ± 0.02defgh
T 30	0.143 ± 0.02defg
T 31	0.14 ± 0.01defg
T 32	0.176 ± 0.01ghij
T 33	0.153 ± 0.01def
T 34	0.133 ± 0.03defghi

Values within column sharing common letter are not significant at $P < 0.05$
values are means ± standard deviation (n=3)

Concentration of lysine obtained with thialysine resistant mutant is presented in table 4.2. Out of 34 mutants only 5 (represented with bold in Table 4.2) showed increased lysine yield, compared to wild type strain, around two fold increase in concentration was observed in the mutants. Mutant T 028 showed maximum concentration of 0.456 g/l.

Table 4.3: Concentration of lysine in thialysine resistant mutants developed from MTCC 2745 strain

Mutants	Lysine concentration (g/l)
Wild type MTCC 2745	0.21 ± 0.02
R 01	0.11 ± 0.02c
R 02	0.20 ± 0.01b
R 03	0.40 ± 0.02a
R 04	0.08 ± 0.01c

Value within column sharing common letter are not significant at P<0.05, values are means ± standard deviation (n=3)

Out of 4 mutants only one showed increased lysine yield and one had almost same concentration. R 03 had maximum production with concentration of 0.4 g/l (Table 4) that is two fold of the wild type strain. Mutants developed from MTCC 2745 strain showed less lysine production as compared to MTCC strain 1815.

4.4 Development of auxotrophic mutants

Thialysine resistant mutants and original wild type strain were used for further development of auxotrophic mutants. These mutants were further treated with UV radiation followed by addition of penicillin to sterilize the prototrophs. Irradiated cell suspension was plated on complete agar medium and on minimal medium plus amino acid for the isolation of the desired auxotrophs. Culture that grew only on Thr + Met containing plates and showed no growth on medium without Thr + Met was selected as auxotroph.

Table 4.5: Lysine concentration of auxotrophic mutants

Mutants	Lysine concentration (g/l)
TA 01	1.2 ± 0.2
TA 02	1 ± 0.25

values are means ± standard deviation(n=3)

Seven colonies were obtained after mutation and only 2 were found to be Thr + Met double auxotrophs. The auxotrophs were then screened. TA 01 and TA 02 showed increased lysine production with concentration of 1.2 and 1 g/l (Table 5). Auxotrophic mutant TA 02 reverted to original type after subculturing. No auxotrophic mutant was obtained with MTCC 2745 strains and thialysine resistant mutant of this strain.

4.5 HPLC Results

To confirm the increase in lysine production, HPLC analysis was performed.

Precolumn derivatization was done with phenylisothiocyanate to form phenylthiocarbamyl amino acid which was used for analysis.

Concentration was calculated by comparing the peak area of standard amino acid solution with sample peak.

Concentration of lysine was calculated as:

$$\text{Conc. of Lysine in g/l} = \frac{\text{Area of sample} \times \text{Dilution Factor} \times \text{Conc. of standard}}{\text{Area of standard} \times 2}$$

Dilution Factor = 100

Conc. of Standard = 0.455 g/l

Table 4.6: Result of HPLC analysis of samples for lysine concentration

Sample	Lysine concentration (g/l)
Wild type (MTCC 1815)	0.10
Thialysine resistant mutant (T 028)	0.20
Auxotrophic mutant (TA 01)	0.63

CHROMATOGRAMS

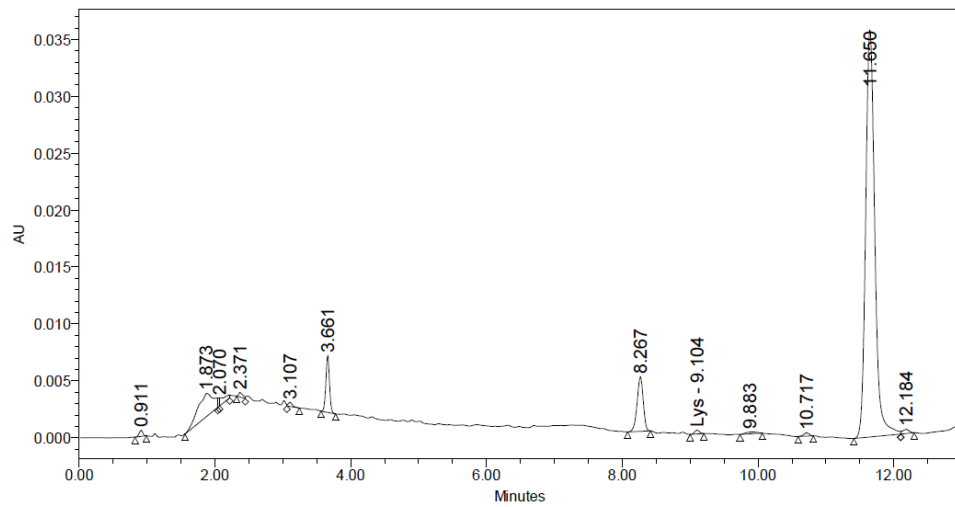


Figure 4.5: HPLC chromatogram for lysine concentration of wild type strain

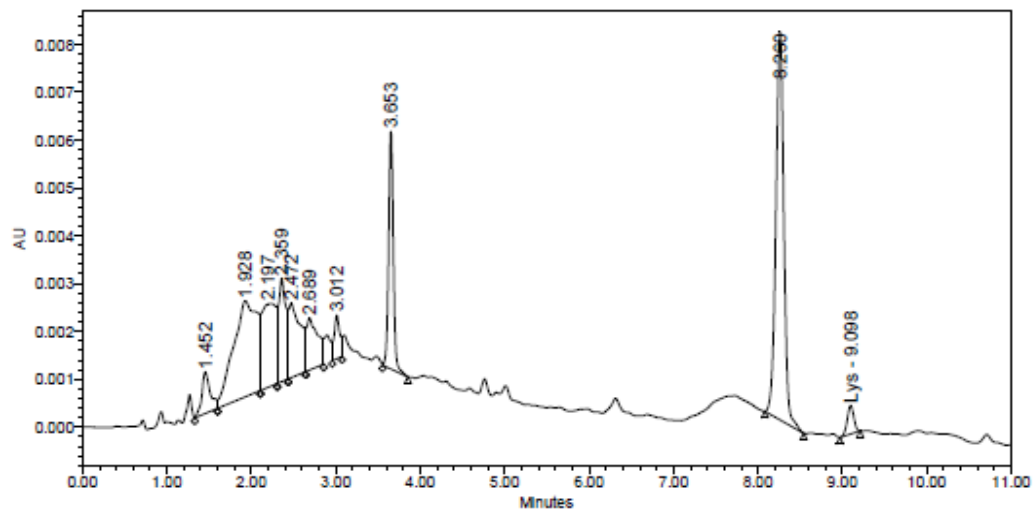


Figure 4.6 : HPLC chromatogram for lysine concentration of thialysine mutant

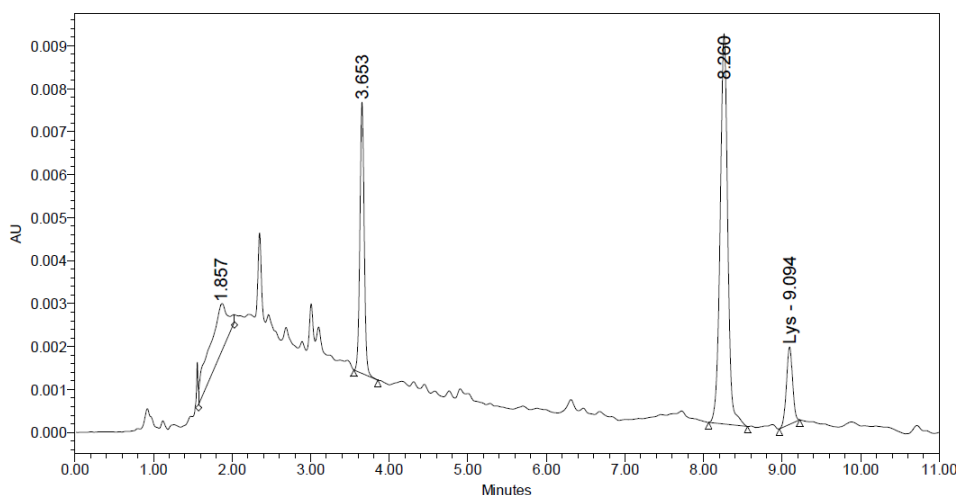


Figure 4.7: HPLC chromatogram for lysine concentration of auxotrophic mutant

In the chromatogram (Figure 4.5, 4.6, 4.7), lysine peaks are represented with Lys name along with the retention time of lysine.

Result of HPLC analysis for lysine concentration in wild type, thialysine resistant and auxotrophic mutants was 0.1, 0.2 and 0.63 g/l.

4.6 Effect of different carbon sources on lysine yield

Carbon sources affect the production of lysine to varying extent in microorganisms. Different carbon sources such as glucose, sucrose, galactose, acetate, lactose were tried for lysine production.

Table 4.7: Concentration of lysine with different carbon sources

Carbon sources	Lysine concentration(g/l)
Glucose	0.2 ± 0.013a
Sucrose	0.11 ± 0.01c
Galactose	0.03 ± 0.002d
Acetate	0.15 ± 0.015b
Lactose	0.02 ± 0.01d

Value within a column with a common letter are not significant at $P < 0.05$
values are means ± standard deviation (n=3)

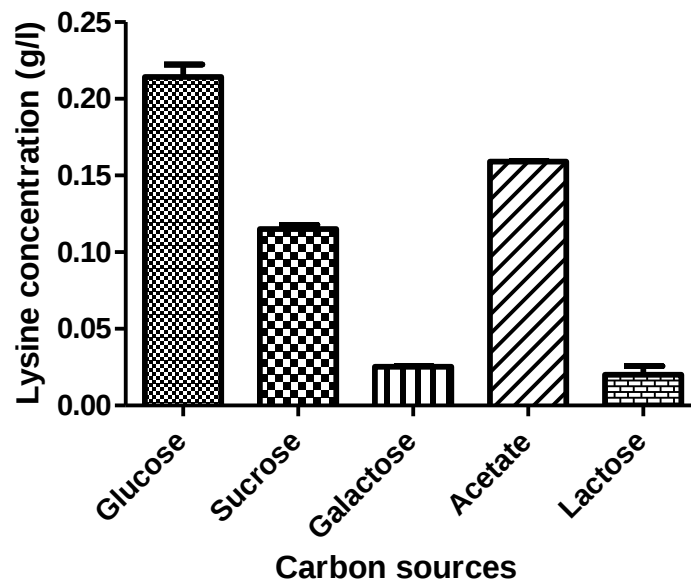


Figure 4.8: Effect of carbon source on lysine production

Maximum lysine yield was obtained with glucose that is 0.2 g/l and minimum with lactose. With sucrose, galactose and acetate, 0.11 0.03 and 0.15 g/l lysine concentration was obtained as illustrated in figure 4.8 and Table 4.7.

Effect of fermentation period

Microorganisms have a specific fermentation period during which they remain viable and produce maximum quantity of metabolites. After a specific period of production and growth, microorganisms start to die and the quantity of metabolite production is decreased to significant amount.

Table 4.8: Effect of fermentation time on lysine production

Fermentation time (in hrs)	Lysine concentration(in g/l)
24	0.1 ± 0.02d
48	0.125 ± 0.01c
72	0.203 ± 0.02a
96	0.188 ± 0.05ab
120	0.178 ± 0.06b

Value within a column with a common letter are not significant at $P < 0.05$
 Values are mean $\pm$ standard deviation (n=3)

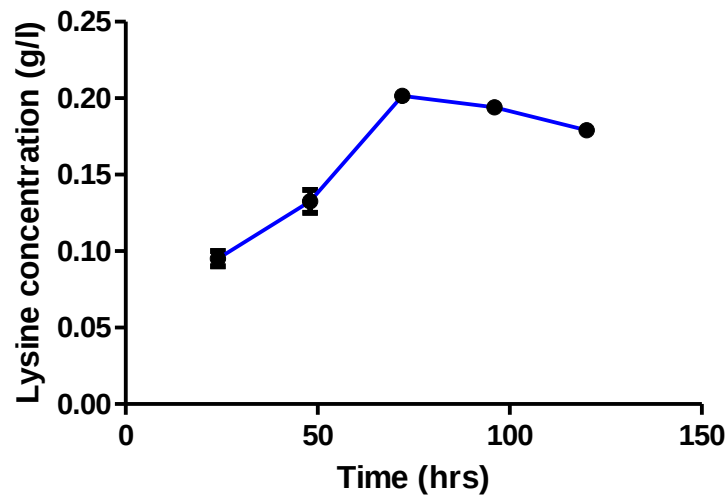


Figure 4.9: Effect of fermentation time on lysine production

Fermentation of lysine was carried out for 120 hrs. Time profile of lysine production has been presented in Figure 4.9. Effect of lysine production with time was that the lysine concentration increased after 48 hrs and was maximum at 72 hrs, after which it almost remained constant and then slightly decreased (from Figure 4.9).

Discussion

Corynebacterium glutamicum was selected for overproduction of lysine in the present study by random mutagenesis. It was observed that wild strain could not produce appreciable amounts of lysine. The main cause of this was the cellular regulation of the metabolic pathway. Regulatory and auxotrophic mutants of the wild strain were developed by random mutagenesis. The aim of developing mutants was to inhibit the feedback control mechanism.

Different mutagens can be used for the desirable changes but UV light was used as a mutagen because of the ratio of mutations with UV are high and is also a safe mutagen (Bridge 1976). In the mutagenesis experiment, 92% lethality was achieved with exposure time of 6 min with UV light. To get the potent mutation 90-99% inactivation is utmost necessity (Kumar et al. 2002). According to this 6 min exposure time was used as the optimum time for inducing mutations.

For overproduction of L-lysine, the most potent mutants are the regulatory or methionine-threonine double auxotrophs. Thialysine (lysine analog) which act as a false feedback inhibitor on aspartokinase (Tosaka *et al*, 1983) was selected for the development of regulatory mutants. Thialysine resistant mutants were developed using thialysine in the minimal media. Thirty four mutants were obtained. Increased lysine yield was obtained in five mutants. Mutant T 28 showed maximum production with a concentration of 0.45 g/l. Shah *et al*. (1999) had reported the development of thialysine resistant mutants for overproduction of lysine and this occurs because of the mutation in the gene of the aspartokinase (lys C), a key enzyme which is feedback regulated by the lysine. Defective aspartokinase in these mutants do not recognize thialysine as lysine and the enzyme remain uninhibited, continue to make aspartyl phosphate and then lysine. These mutants did not respond to intracellular lysine levels and therefore continue to synthesis lysine.

In rest twenty nine mutants, production of lysine was found to be less as compared to wild type strain. In these mutants, there might be no mutation in the aspartokinase gene due to which thialysine was recognised as lysine, and the enzyme was inhibited as if lysine had accumulated in the cell.

Shah *et al*. (1999) had reported that thialysine resistant mutant did not produce enough due to the concerted feedback inhibition, therefore blockage of side reactions that lead to

threonine and methionine synthesis is also needed, for this threonine-methionine double auxotroph were developed.

The frequency of occurrence of auxotroph by simple UV light was very low. So enrichment with penicillin after UV treatment was carried out. Saito and Ikeda (1957) reported that penicillin sterilizes actively growing cells by blocking the cell wall synthesis, therefore only auxotroph mutants survive after this treatment and penicillin was destroyed with penicillinase which allowed the growth of auxotroph in the supplemented media containing methionine and threonine. As a result the double auxotroph were obtained.

One threonine and methionine double auxotroph was isolated which showed increase lysine production as compared to thialysine resistant mutant and wild type strain. Increased in yield was obtained with double auxotroph because homoserine dehydrogenase and aspartokinase are inhibited by threonine present intracellularly, due to which all the aspartyl phosphate formed is channelled to lysine production.

Effect of fermentation time on lysine production was studied by estimating the lysine concentration after every 24 hrs, it was determined from the results that exponential phase of cell growth of *C. glutamicum* was completed within 24 hours of fermentation. The production rate was maximum between 48 to 72 hours, after which it almost stopped (production phase). Pham *et al.* (1993) and Matos and Coello (1999) observed that maximum lysine production in 48 to 72 hours and lysine fermentation was completed in two different time phases; first, physiologic state of growth and second, lysine production phase. They also observed that most of the carbon source was consumed in the first phase of fermentation.

Effect of carbon source was studied to find the best substrate for maximum lysine production. It was found that maximum lysine was obtained with glucose as carbon source. Ferreria and Durate (1991) utilized glucose for the highest yield of L-lysine by *Corynebacterium glutamicum*. Biotin is mandatory for the appropriate synthesis of L-lysine. Young and Chipely (1984) explored the outcome of biotin on L-lysine fermentation in the *Brevibacterium lactofermentum*, and it was observed that biotin treated cell built up more glucose than the untreated one. Biotin actually induced a few modifications in the composition of cell wall, permitting an enhancement in accumulation of sugar. The uptake studies reveal that biotin affects the cell surface probably the bacterial membrane. Tosaka *et al.* (1986) suggested this effect might be due to activation of pyruvate carboxylase by biotin.

Sucrose and acetate showed higher yield as compared to lactose. Shio *et al.* (1990), Woo *et al.* (2010) have studied that sucrose uptake occurs via a phosphotransferase system, where sucrose is phosphorylated at the glucose ring followed by invertase catalysed hydrolysis into glucose-6-phosphate and fructose. The acetate utilization involves its uptake and subsequent activation to acetyl coenzyme A (acetyl-CoA) which then directly enters the citric acid cycle. Lowest yield was observed with lactose and galactose as the enzymes catalysing the conversion of these carbon sources to glucose are absent in *Corynebacterium glutamicum*.

Conclusion

Treatment of cells by UV light for 6 min was sufficient to cause lethality and induce mutations.

Auxotrophic mutants were derived from the parent strain of *Corynebacterium glutamicum* and showed higher lysine production (0.6 g/l), which was six fold as compared to wild type strain. This indicates that in the mutant aspartokinase became insensitive to concerted feedback inhibition by lysine and threonine due to the mutations induced by UV light.

Regulatory mutants developed by random mutagenesis (UV light) followed by selection with lysine analog (thialysine) did not show much improvement in lysine yield as compared to auxotrophs, this showed that application of analog is not a sufficient criteria for development of lysine overproducing mutants. Lysine concentration in these mutants was 0.2 g/l.

Highest yield of L-lysine was obtained in glucose medium as compared to other Carbon sources (acetate, sucrose, galactose, lactose) Maximum lysine production was obtained between 48-72 hrs.

SUMMARY

Amino acids have now been produced with the aid of microorganisms for nearly 50 years. The economic importance of these cellular building blocks is significant, hence, demand is continually growing and constant efforts to increase production are directed towards the microorganism. The highest produced amino acid is L-glutamic acid, followed by L-lysine and DL-methionine. The reason for the increased demand for amino acids stems from their utilization as food additives, feed supplements, therapeutic agents and precursors for the synthesis of peptides or agrochemicals. L-Lysine is required as a feed additive for poultry and pig breeding.

Up until the 1950s no appropriate commercial process for production of natural l-amino acids existed except by isolation from natural proteins. For that reason, continuous efforts were made in order to improve the nutritional value of low cost vegetable proteins by enrichment with essential amino acids. In 1957, Kinoshita *et al.* discovered a potent amino acid-producing microorganism, *Corynebacterium glutamicum* (initially named *Micrococcus glutamicus*), which provided a novel method for producing natural amino acids. *C. glutamicum* is a Gram-positive, non-sporulating bacteria. It is not motile, with pleomorphic short rods (0.7–1×1–3) μm in size producing yellowish colonies and having a DNA G + C content of 53–55%. It requires biotin in order to grow, cultivation temperatures of approximately 30°C, with most strains able to utilize acetic acid, glucose or sucrose for amino acid production.

When compared to chemical methods, fermentative production has the advantage of yielding the optically active and biologically required L-form of amino acids from cheap carbon and nitrogen sources. Extensive research has been made in order to improve the fermentation process not only from the point of lowering production costs but also of increasing the productivity. Improvements include increased yield of desired metabolites, removal of unwanted cometabolites, as in case of lysine, methods have been developed to increase lysine yield by inhibiting the synthesis of threonine and methionine (cometabolites). Attempts in strain improvement have mainly been directed towards regulating the corresponding pathways via classical mutagenesis and screening methods. Nowadays, most amino acids are in fact produced by the use of mutants that contain combinations of auxotrophic and regulatory mutations.

Lysine biosynthesis is well controlled in *C. glutamicum* through enzymes by feedback inhibition and repression mechanisms. Intracellular lysine and threonine cease the activity of aspartokinase by concerted feedback inhibition. Thus conversion of aspartate to aspartyl phosphate is being stopped. Another important enzyme on the way is homoserine dehydrogenase which is inhibited by L-threonine and repressed by L-methionine.

Lysine production was increased by developing regulatory and auxotrophic mutants. Initially UV exposure time was optimised to achieve 90-99% lethality required for inducing mutations. UV dose of 30 J/m² was given for different time intervals. 92% lethality was achieved with 6 min of exposure.

Regulatory mutants were isolated by random mutagenesis via UV exposure of 6 min followed by selection with thialysine (lysine analog) in the minimal media. Mutants obtained were screened for lysine concentration by ninhydrin ferric reagent method and also by HPLC. Mutants showed two fold increase in lysine production as compared to wild type strain. Thialysine acted as pseudo false feedback inhibitor.

Further increase was obtained with development of double auxotrophic mutants (threonine and methionine auxotroph). These mutants were isolated in minimal media plus threonine and methionine. Six fold increase was found in these mutants as compared to wild type and two fold as compared to thialysine mutants. In auxotrophic mutants both the key enzymes (aspartokinase and Homoserine dehydrogenase) was mutated as a result of which there was no feedback regulation in the lysine pathway and increase production occurred.

Lysine production was assayed after every 24 hrs for 120 hrs to found the time when maximum concentration of lysine can be obtained. It was found that between 48-72 hrs there was maximum production. Glucose was best carbon source as compared to sucrose, acetate and galactose to have maximum lysine production.

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